

基于悬垂平板偏转角的明渠流量估算模型及验证

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摘要:针对平板量水设施缺乏适用性广泛的流量计算模型, 该文从2个角度提出流量估算模型, 首先分析绕轴自由旋转薄平板在水中的受力, 根据升力简化为竖直方向静水压力设想, 提出压力体计算假设, 根据动量定理与力矩平衡公式得到了流量、角度、水深三者的理论关系式, 通过U型和矩形渠道进行试验, 验证假设合理性; 根据闸孔出流流量公式针对矩形渠道建立闸孔出流半径验计算模型, 拟合得出半径验流量公式。对于第1种模型, 对于U型渠道, 2种压力体假设均适用于流量计算, 除流量小于10 L/s时, 相对误差超过10%, 其他均小于10%, 流量大于17 L/s时误差均在5%左右; 对于矩形渠道, 仅假设1适用流量计算, 假设2不成立, 应用假设1计算压力体时, 当流量较小(10 L/s左右)时的个别工况误差会偏大, 大部分工况下计算误差均小于10%; 对于闸孔出流计算模型, 计算流量与实测流量之间最大误差不超过18%, 大部分工况下计算误差在10%以下。当悬垂薄平板与明渠横断面等大时, 来流量与偏转角度存在单值对应关系, 角度随着来流量的增大而增大; 同一流量下, 板前后水深比、板前与下游水深比分别与偏转角度呈现出单独的函数关系, 板前后水深比、板前与下游水深比随着平板偏转角度的增大而减小, 但减小幅度变缓。对于不同流量, 板前后水深比、板前与下游水深比随着角度增大而增大, 但增大幅度变缓。研究可为灌区量水设施设计及应用提供新思路。

关键词:渠道; 角度; 流量; 绕流阻力; 受力方向; 闸孔出流

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0 引言

灌区量水技术作为实现灌区水资源优化配置和现代化农业用水管理的基本手段, 为灌区用水的水费收取提供依据, 提高农户节约用水意识^[1-6]。置于明渠中可定轴转动的平板制作方便, 测流时造成的水头损失小, 水体冲击平板造成的角度偏转可以用来估算流量。目前关于平板绕流的研究多以完全浸入流体中平板的运动为主, 探究放置平板攻角、雷诺数、平板尺寸参数等对其尾涡脱落特性, 绕流阻力大小及阻力系数的影响。贾文超^[7]根据流体力学基本理论, 改进双向流固耦合算法, 依次对二维平板、二维翼型、三维翼型的涡激振动特性作出分析, 对频率锁定现象进行研究。秦义^[8]通过流固耦合的方法, 分析了

平行于来流与垂直于来流放置转动板以及这两种板的组合板在高雷诺数下, 不同运动频率和振幅下的旋转振荡绕流问题。张青山^[9]分别在水槽和风洞中对平板分离再附流动的流场进行细致的试验测量, 研究了不同弦厚比下平板分离再附流动的非定常特性和隐藏在分离剪切层内的大尺度旋涡结构的发展变化以及其与壁面脉动压力之间的联系。姜海波等^[10]根据垂直平板绕流阻力和对称薄翼型全攻角绕流试验, 研究得到平板大攻角放置时绕流总压力与升力和阻力分量系数与攻角的半经验计算公式。

对于平板绕流装置的研究, 目前多从力、动量和量纲的角度进行研究, 拟合得到经验公式。Tariq等^[11-13]研究绞杆在水中的偏转现象, 得到半经验平均流速关系式, 并对细杆速度系数的影响因素进行分析; 刘力奂等^[14-15]根据泵站拍门受力计算理论, 提出半经验角度流量关系式, 并对其中待定流量系数取值进行验证。王军等^[16-17]设计板式测流设施, 并对半经验公式中的待定系数影响因素进行分析。石先德等^[18-19]对摆杆式测流装置进行水力性能试验研究, 结合数值模拟对其测流精度进行分析。中国北方灌区渠道底坡缓, 灌溉水流多泥沙, 在保证量水精度

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要求的条件下需采用结构简单、过流能力强、水头损失小的量水设施;平板量水设施施测简捷,过流能力强,但受制于渠道体型、坡度、平板本身材质等因素,使其缺乏适用性广泛的流量计算模型,难以广泛应用灌区量水。因此,本文从绕流理论和闸孔出流2个角度出发,在U形和矩形渠道进行原型试验,对悬垂平板在绕流中的受力做出分析,由于板后绕流存在水位差,浮力可以看做静水压力一部分,所以仅将升力简化为静水总压力竖直分力,结合原型试验,验证渠道流量与悬垂平板偏转角的关系式;基于前人对弧形闸门过流计算及自动闸门的研究^[20-27],观察试验水流流态,提出以闸孔出流流量计算模型为基础的半径经验流量公式,旨在为平板量水装置的实际应用提供理论依据。

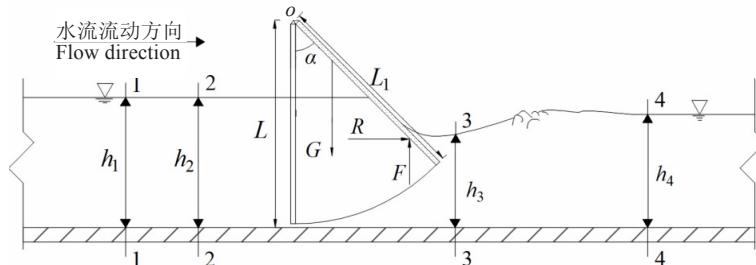
1 理论分析

在实际流体发生绕流过程中,绕流物体所受水流作用力可以转化为竖向升力F与水平绕流阻力R。绕流阻力由

摩擦阻力和压差阻力构成。摩擦阻力主要由物体表面边界层中水体运动状态决定,由水体的黏滞力主导。压差阻力大小是由绕流物体形状决定,由于平板为非流线型物体,在水体绕经平板时,在平板的边缘会发生边界层的分离,从而导致尾涡脱落,由于绕流的能量损失及压能对动能的补偿,使板前后出现压差形成阻力。本文试验中明渠流的雷诺数较大,黏滞力作用小,摩擦阻力对于计算结果影响较小,故忽略。通过前期试验观察,水体绕过平板时,平板前后会形成明显的水位差,故假设升力是静水总压力垂直分力(压力体),研究在绕流现象中偏转角度和来流量之间的关系。

1.1 力矩平衡与动量方程

于明渠渐变流中安置悬垂薄平板(薄平板形状和渠道横断面尺寸相似,以U型渠道为例,见图1),平板可以绕固定轴O自由转动,薄平板在重力G,绕流阻力R和竖向升力F作用下,绕轴O偏转角度α,达到平衡。



注: h_1 为上游断面稳定水深, m; h_2 为板前断面稳定水深, m; h_3 为水流紧贴板后断面水深, m; h_4 为下游稳定水深, m; L 为轴 O 至渠底中心的垂直距离, m; L_1 为轴 O 到平板末端的长度, m; α 为偏转角度, ($^\circ$); G 为平板重力, N; R 为绕流阻力, N; F 为升力, N。

Note: h_1 is flow depth of upstream section, m; h_2 is flow depth in the front section, m; h_3 is flow depth clinging to plate, m; h_4 is steady flow depth of downstream section, m; L is the vertical distance from O to the center of the canal bottom, m; L_1 is the distance from O to the end of plate, m; α is deflecting angle, ($^\circ$); G is gravity of plate, N; R is flow resistance, N; F is lift force, N.

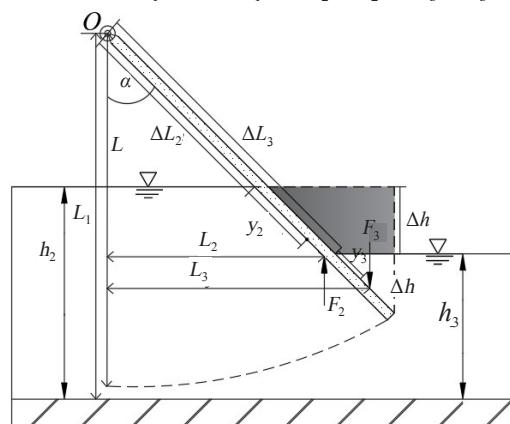
图 1 平板受力分析

Fig 1. Schematic diagram of stress analysis of plate

本文在计算升力时,将其简化为竖直向上水压力, F 的值与压力体大小有关, 压力体由板前后水位差产生的竖直分力 $F_2 - F_3$ (图2灰色部分)组成(统称为假设1):

$$\text{升力 } F: \quad F = F_2 - F_3 \quad (1)$$

$$\text{升力产生力矩 } M_F: \quad M_F = F_2 \cdot L_2 - F_3 \cdot L_3 \quad (2)$$



注: F_2 为板前水深 h_2 产生竖向升力, N; F_3 为板后水深 h_3 产生竖向静水压力, N; ΔL_2 为 L 与平板迎水面没入水下部分之差, m; ΔL_3 为 L 与平板背水面没入水下部分之差, m; y_2 是平板迎水面没入水流部分面积的形心沿平板偏转方向延伸至板前水面的直线距离, m; y_3 是板体背水面没入水流部分面积形心沿板方向延伸至板前水面的距离, m。

Note: F_2 is vertical hydrostatic pressure caused by h_2 ; F_3 is vertical hydrostatic pressure caused by h_3 ; ΔL_2 is difference between L and length of flat upstream face under water, m; ΔL_3 is difference between L and length of flat downstream face under water, m; y_2 is distance between centroid of flat upstream face under water and water surface, m; y_3 is distance between centroid of flat downstream face under water and water surface, m.

图 2 升力 F 组成

Fig 2 Composition of lift force

其中:

板前水深 h_2 产生竖直方向静水压力 F_2 :

$$F_2 = \rho \cdot g (y_2 \cdot \cos\alpha) A_2 \cdot \sin\alpha \quad (3)$$

F_2 对轴 O 的力臂 L_2 :

$$L_2 = (\Delta L_2 + y_2 + \frac{I_{C_2}}{y_2 \cdot A_2}) \cdot \sin\alpha \quad (4)$$

$$\Delta L_2 = L - \frac{(L_1 - h_2)}{\cos\alpha} \quad (5)$$

式中 A_2 为平板迎水面浸入水体的面积, m^2 ; α 为平板偏转角度, ($^\circ$); ρ 为水的密度, 10^3 kg/m^3 ; y_2 为 A_2 形心沿板偏转方向延伸至板前水面的直线距离, m; I_{C_2} 为 A_2 对通过其形心垂直于水流方向上的惯性矩, m^4 ; h_2 为平板前稳定水深, m, L 为平板末端到轴 O 的距离, m; L_1 为渠底到轴 O 的垂直距离, m; ΔL_2 为 L 与平板迎水面没入水下长度之差, m; g 为 9.8 N/m^2 。

板后水深 h_3 产生竖直方向静水压力 F_3 :

$$F_3 = \rho \cdot g (y_3 \cdot \cos\alpha) A_3 \cdot \sin\alpha \quad (6)$$

F_3 对轴 O 的力臂 L_3 :

$$L_3 = (\Delta L_3 + y_3 + \frac{I_{C_3}}{y_3 \cdot A_3}) \cdot \sin\alpha \quad (7)$$

$$\Delta L_3 = L - \frac{(L_1 - h_2 + \Delta h)}{\cos\alpha} \quad (8)$$

式中 A_3 为平板背水面浸入水体的面积, m^2 ; y_3 为 A_3 形心沿

板偏转方向延伸至板前水面的直线距离, m; I_{c_3} 为 A_3 对通过其形心并与垂直于水流方向上的惯性矩, m^4 ; h_3 为板后水深, m, L 为平板末端到轴 O 的距离, m; L_1 为渠底到轴 O 的距离, m; ΔL_3 为 L 与平板背水面深入水下部分之差, m。

绕流阻力 R 对轴 O 的力矩 M_R :

$$M_R = R \cdot L_R \quad (9)$$

$$L_R = (\Delta L_2 + y_2) \cdot \cos\alpha \quad (10)$$

式中 R 为绕流阻力, N, 并假设作用点在平板迎水面浸入水体面积 A_2 形心上, L_R 是 M_R 力臂, m。

重力 G 对定轴 O 的力矩 M_G :

$$M_G = G \cdot L_G \quad (11)$$

式中 G 为平板重力, kg; L_G 是 M_G 力臂, m。

对平板列力矩方程:

$$G \cdot L_G = R \cdot L_R + F \cdot L_F \quad (12)$$

式中 L_F 代表升力 F 产生力矩 MF 的力臂, m。

选取断面 1-1、4-4 间水体为控制体, 当流量稳定后, 控制体内水流运动可视为恒定流。故动量方程:

$$\rho Q(\beta_4 v_4 - \beta_1 v_1) = P_1 - P_4 - R \quad (13)$$

$$P_1 = \rho g h_{c1} A_1 \quad (14)$$

$$P_4 = \rho g h_{c4} A_4 \quad (15)$$

式中 v_1 、 v_4 分别为渐变流断面 1-1、4-4 的平均流速, m/s; P_1 、 P_4 分别为断面 1-1、4-4 的动水压力, N; h_{c1} 、 h_{c4} 分别为过水断面 1-1、4-4 的形心点水深, m; A_1 、 A_4 为过水断面 1-1、4-4 的面积, m^2 。由于两断面水流流线近似平行, 动水压力取为静水压力: 根据流体中点应力状态分析^[28]可知, 理想流体一点压强任意方向大小相等, 且与黏性流体中平均点压强之差 $p - p' = (\lambda + \frac{2}{3}\mu) \nabla \cdot v = \mu_v \nabla \cdot v$, 明渠水流为不可压缩流体, 故 $\nabla \cdot v = 0$, $\lambda = -\frac{2}{3}\mu$, 所以 $p = p'$ 。 μ 为流体黏性系数, λ 为膨胀黏性系数。

根据式(2)、式(9)~式(15)得到式(16)

$$Q = \left[\frac{\rho \cdot g (h_{c1} A_1 - h_{c4} A_4) - \frac{G \cdot L_G - (F_2 \cdot L_2 - F_3 \cdot L_3)}{L_R}}{\rho \left(\frac{\beta_4}{A_4} - \frac{\beta_1}{A_1} \right)} \right]^{0.5} \quad (16)$$

式(16)中, β_1 、 β_4 为动量修正系数, 一般渐变流中动量修正系数值约为 1.02~1.05^[28], 为简化计算, 取值为 1。由于所选控制体长度较短, 忽略渠底对水流的摩擦阻力, 并取上游水位与板前水位相等。由分析过程知, 当渠道断面形状, 平板密度及厚度已知时, 渠道来流量与平板偏转角度具有一一对应关系。

对式(16)进行量纲分析, 如式(17)所示, 满足量纲和谐。

$$[L^3 T^{-1}] = \left[\frac{[L^{-3} M] \cdot [L T^{-2}] \cdot L^3 - \frac{ML^2 T^{-2}}{L}}{[L^{-3} M] \cdot L^{-2}} \right] = [L^3 T^{-1}] \quad (17)$$

1.2 闸孔出流流量计算模型

闸孔出流水力计算是在一定闸前水头下计算不同闸孔开度时的泄流量, 而闸孔出流流态影响着流量系数的取值, 正确分析流态特征, 确定出流条件对流量的准确计算有着重要意义。在试验时发现平板后水流流态与淹没出流下的闸孔出流流态相似, 因此以闸孔出流流量计算模型为基础, 拟合得到流量系数的经验表达式, 得到流量与偏转角度的半经验关系式。

对上下游渐变流断面列能量方程^[28]得:

$$h_1 + \frac{v_1^2}{2g} = h_4 + \frac{v_4^2}{2g} + \xi \frac{v_1^2}{2g} \quad (18)$$

式中 h_1 为上游渐变流断面水深, 因上游水深与板前断面水深相近, 默认相等; h_4 为下游渐变流断面水深, m; v_2 、 v_4 分别为断面平均流速, m/s; ξ 为局部水头损失系数。

1-1 断面处水流平均流速:

$$v_1 = \frac{1}{\sqrt{\xi - 1}} \sqrt{2g(h_1 - h_4) - v_4^2} = \frac{1}{\sqrt{\delta + \xi - 1}} \sqrt{2g(h_1 - h_4)} \quad (19)$$

开度 e :

$$e = L - L_1 \cos\alpha \quad (20)$$

式(19)~(20)中 e 为偏转时平板开度, m; $\delta = v_4/v_1$ 。

$$Q = A_1 v_1 = \frac{be}{\sqrt{\delta + \xi - 1}} \sqrt{2gh_1} = \mu_s b e \sqrt{2gh_1} \quad (21)$$

式中 A_1 为 1-1 断面中平板部分水流过水断面面积, m^2 ; μ_s 为流量系数; Q 为总流量, L/s; b 为矩形渠道宽度, m。

2 原型试验

2.1 试验布置

试验系统(见图 3)主要包括稳水格栅, 水泵, 三角形量水堰, 流量调节阀门, 电磁流量计, 尾门, U 形渠道, U 形平板, 矩形渠道, 矩形平板等。试验测点布置图见表 1。

表 1 测点布置

Table 1 Layout of measuring points

测点 Measuring points	距 U 形渠道进口的距离 Distance from U-shaped canalhead /cm	距矩形渠道进口的距离 Distance from rectangular canal head/cm
1	300	350
2	450	400
3	紧贴板	430
4	580	440
5	640	紧贴板
6	680	530
7	740	560
8	800	600
9	900	630
10	—	650
11	—	700
平板安装位置 Plate placement	500	450

U 形渠道为标准 D40 渠道(图 3), 由有机玻璃材料制成, 渠道坡度 5×10^{-3} , 综合糙率 0.011; U 形平板为铝制, 板厚 8 mm, 为减小不必要的误差, 安装时使平板顶部和渠道顶部平齐, 平板边缘距渠道侧壁及底部均为 1 cm。

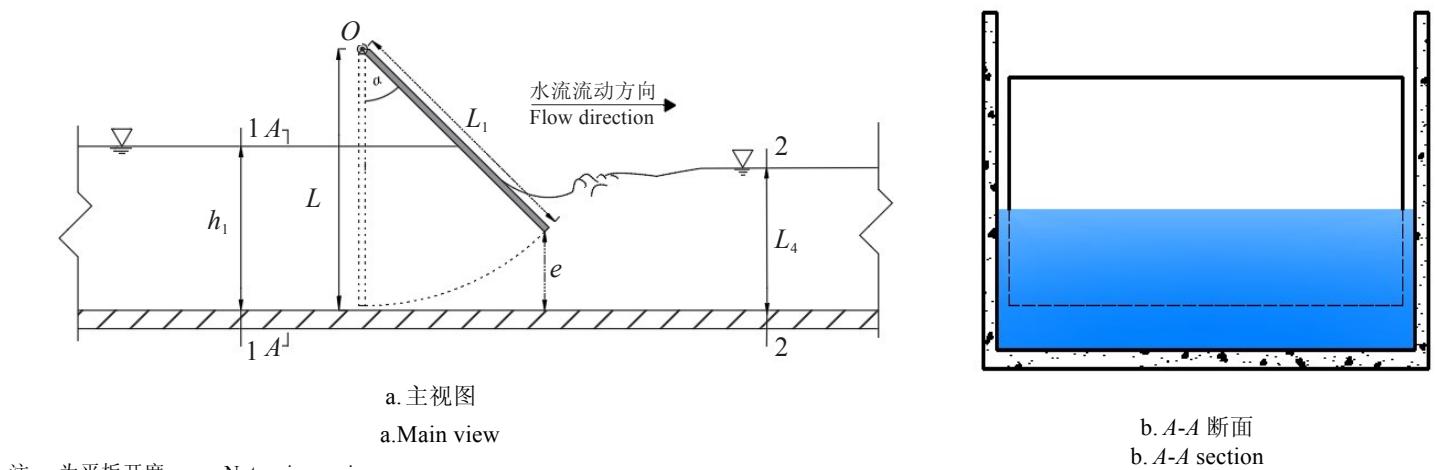


图3 梯道横断面示意图
Fig 3. Schematic of canal section

矩形渠道由混凝土衬砌而成(图4),底坡是平坡,综合糙率0.014;矩形铝制平板板厚5 mm,安装时使平板侧边缘距离渠道侧壁1 cm,板底距渠底5 mm。

平板偏转角度用电子数显角度尺测量,精度0.1°;断面水深用水位测针测量,精度0.1 mm。U型平板试验流量范围9~44 L/s,共选取9个流量,每种工况流量相差5 L/s左右;矩形平板试验流量范围为10~40 L/s,共5种流量,每种流量下改变尾门调节水深4次,共20种工况;每种流量下水深及偏转角测量多次。

2.2 结果与分析

2.2.1 流量-偏转角度关系验证

选取所测角度及水深代入式(16),得出理论值。文献[29]在计算升力时,将板体体积产生的浮力加入到压力体的计算中(统称为假设2)。图5a给出了平板在U型渠道中2种假设下,实际流量及计算流量的相对误差。图5b给出的是矩形渠道假设1计算流量与实测流量的相对误差。对于U型渠道,2种压力体假设均适用于流量计算,除流量较小时,相对误差超过10%,其余工况流量大于17 L/s时,相对误差均在5%左右。对于矩形渠道,经验证,应用假设2计算压力体时(图5c)计算流量与实际流量相对误差较大,应用假设1计算压力体时,当流量在10 L/s左右时误差会偏大,除个别工况计算误差大于10%外,大部分工况下计算误差均小于10%。从计算结果看出,本文中所提假设1适用性强于假设2。

2.2.2 阀孔出流流量计算模型

闸孔出流流态不同影响着流量系数的取值,经计算发现板后断面傅汝德数始终小于0.5,板后水流流态与完全淹没出流下水流流态相似^[20],故采用闸孔出流淹没出流流量计算模型进行半径验拟合。联立式(20)和式(21):

$$Q = \mu_s b e \sqrt{2gh_1} = \mu_s (L - L_1 \cos\alpha) b \sqrt{2gh_1} \quad (22)$$

式中 μ_s 为流量系数; b 为矩形渠道宽度,m; e 为开度,m; L 为轴O到装置末端距离, L_1 为轴O到渠底距离,m。

通过图6可以看出所有工况下的 $(h_1/h_4, u_s)$ 密集的分布在1条曲线周围,得出流量系数计算模型:

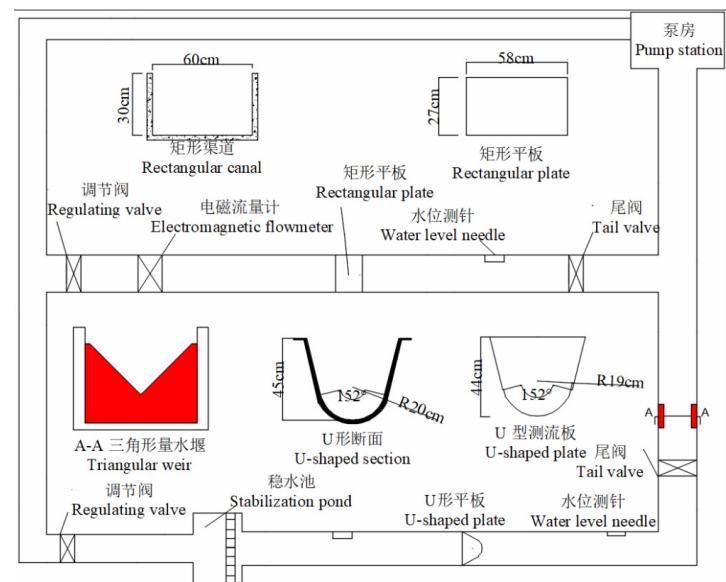


图4 试验布置图
Fig. 4 Layout plan

$$\mu_s = k \left(\frac{h_1}{h_4} \right) + b \quad (23)$$

式中 k, b 为参数,由板型和渠道尺寸决定。

由此拟合得出半径验流量公式:

$$Q = f(h_1, \alpha) = \mu_s b_1 e \sqrt{2gh_1} = \left[1.9283 \left(\frac{h_1}{h_4} \right) - 1.7502 \right] (L - L_1 \cos\alpha) b_1 \sqrt{2gh_1} \quad (24)$$

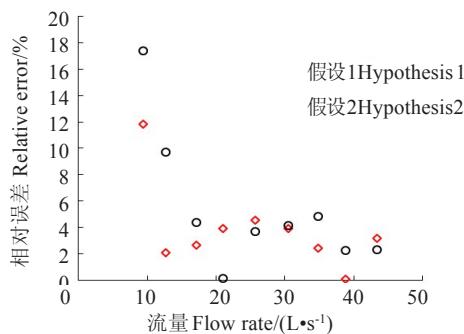
将计算值与实测值对比(图6b)。结果表明:二者之间最大误差不超过18%,大部分工况下计算误差在10%以下。公式中没有出现板后水深 h_3 ,相比理论模型,在实践中应用性更强。

2.2.3 平板偏转角度水深关系讨论

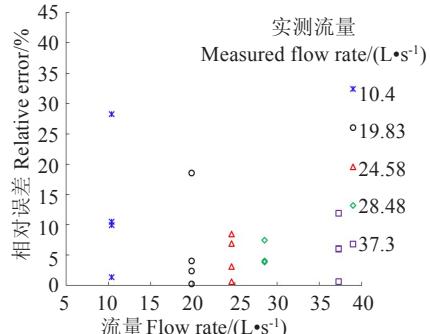
图7为矩形渠道试验工况下板前后水深比、上下游水深比与偏转角度 α 的关系。

从图7可以看出,同一流量下, h_1/h_4 、 h_1/h_3 分别与偏转角度 α 有着单独的函数关系, h_1/h_4 与 h_1/h_3 随着平板偏转角度的增大而减小,但减小幅度变缓。对于不同流量,随着流量的增大, h_1/h_4 与 h_1/h_3 随着角度增大而增大。由第

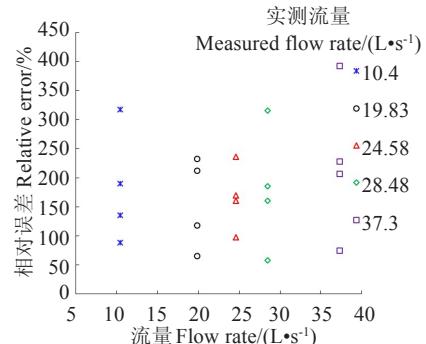
一种流量关系式的推导可知, Q 可转化为 h_1 与角度 α 的函数, 其形式可表示为 $Q=f(h_1, \alpha)$, 这与文献[11]得出的结果



a. U形渠道验证
a. Verification for U-shaped canal



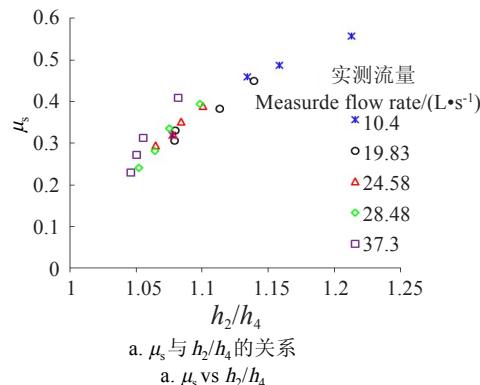
b. 矩形渠道假设 1 验证
b. Hypothesis 1 verification for rectangular canal



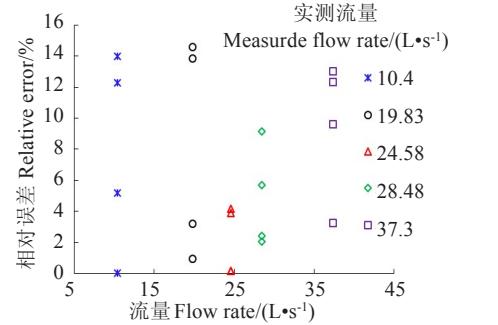
c. 矩形渠道假设 2 验证
c. Hypothesis 2 verification for rectangular canal

图 5 计算流量与实测流量相对误差

Fig 5 Relative error between calculated and measured flow rate



a. μ_s vs h_2/h_4



b. 实测流量与计算流量相对误差
b. Relative error between calculated and measured flow rate

注: μ_s 为流量系数; h_2/h_4 为板前水位与下游水深比。

Note: μ_s is discharge coefficient; h_2/h_4 is value of flow depth in the front section divided by flow depth of downstream section.

图 6 经验公式验证
Fig 6 Verification of empirical formula

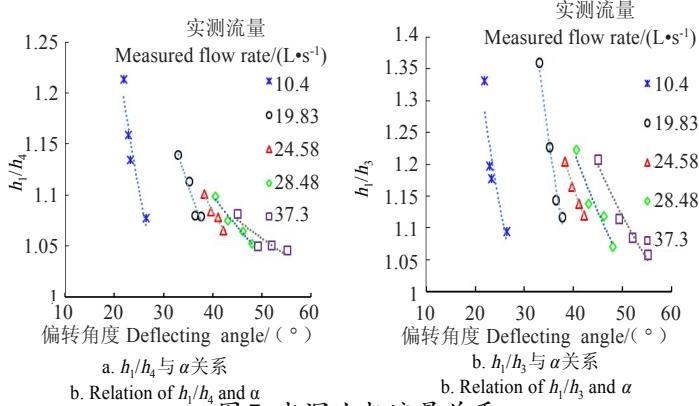


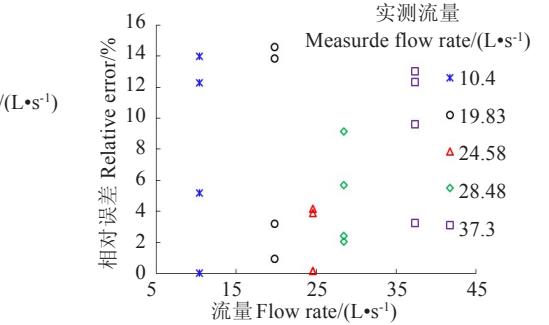
图 7 水深比与流量关系

Fig 7 Relationship between depth ratio and angle

3 结论

1) 根据升力简化为竖直方向静水压力设想, 提出 2 种压力体计算假设, 根据动量定理与力矩平衡公式得到了流量、角度、水深三者的理论关系式, 并验证假设合理性。对于 U 型渠道, 2 种压力体假设均适用于流量计算, 除小流量工况验证时相对误差大于 10%, 当工况流量大于 17 L/s 时, 相对误差均在 5% 左右; 对于矩形渠道, 仅假设 1 适用流量计算, 假设 2 不成立。应用假设 1 计算压力体时, 当流量在 10 L/s 左右时误差会偏大, 除个别工况计算误差大于 10% 外, 大部分工况下计算误差均小于 10%。因此本文提出的假设 1 适用性更强, 测流范围在 10~44 L/s。

类似, 可以此作为切入点, 对平板量水设施流量角度关系进行更进一步探究。



a. h_1/h_4 与 α 的关系
a. Relation of h_1/h_4 and α

2) 由于板后水流流态与完全淹没出流流态下水流流态相似, 根据闸孔出流流量公式建立半经验计算模型, 拟合得出半经验流量公式。结果表明: 计算流量与实测流量之间最大误差不超过 18%, 大部分工况下计算误差在 10% 以下。公式中没有出现板后水深 h_3 , 在实践中应用性更强。

3) 同一流量下, 板前后水深比 h_1/h_4 、板前与下游水深比 h_1/h_3 分别与偏转角度 α 呈现出单独的函数关系, h_1/h_4 与 h_1/h_3 随着平板偏转角度的增大而减小, 但减小幅度变缓。对于不同流量, h_1/h_4 与 h_1/h_3 随着角度增大而增大, 但增大幅度变缓。

本文从 2 个角度对平板量水的测流机理进行探讨。由于在试验中无法在同一时刻对所涉及物理参数进行同时测量, 理论模型中下游水深 h_4 对计算结果影响较大, 应考虑在公式中加入“随机项”及修正函数来对其进行修正。

水力自动闸门是根据上游来水量及水位变化, 利用水压力产生的推动力矩与闸门及配重产生的回复力矩进行自动启闭, 实现水流的自动调节的闸门。类似挡板结构的自动闸门在国外灌区的应用已取得一定研究成果。闸门宽度并非与断面宽度一致, 采用闸孔出流公式和宽顶堰流公式分别对闸门下流量和两侧绕流流量进行半经验计算, 既能提高过流能力, 也可以实现流量的测控。但是

中国北方渠道底坡较平缓,灌溉水流含沙量大,闸前堰坎的存在会造成严重的泥沙淤积,影响渠道的输水能力。本文设计平板板型与断面大小一致,可参考国外挡板闸门结构,将运动水流分区进行分析,并且改变平板收缩比,将板后形状改为圆弧形,添加平衡锤,使得板后水压力对圆心力矩为0(水压力垂直于作用圆弧面,对圆心取矩),进而通过力矩平衡原理进行简化计算。该量水设施有望结合电子设施实现对渠道流量的远程动态监测。目前该量水装置仅在清水条件下进行了试验,当水流含有泥沙时,泥沙含量会使平板受力有所变化,使平板偏转角与流量的关系与清水工况不同,假设合理性尚需进一步试验研究。

该文仅针对当平板尺寸与渠道等大时,对平板偏转角与来流流量关系进行探讨,计算模型仍需进行完善。当平板面积与渠道尺寸不一致时,水流绕流作用加剧,平板角度流量影响因素均不相同,仍需对模型中假设进行进一步验证。

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Flow estimation model and verification based on deflection angle of dangling plate in open channel

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Abstract: In view of lack of effective regional water measuring facilities for gentle slope canal with silt current in irrigation areas of northern China, a portable flat water measuring device was proposed as a flow water measuring equipment in the field. Many factors such as canal sizes, slopes and flat plate materials are related to the device, thus a widely applicable flow calculation model was needed. This study was to research its hydraulic performance of plate water measuring facilities based on prototype test carried out in Northwest A & F University in Yangling, Shannxi of China. In order to explore dynamic characteristics and deflection phenomenon of a draping thin plate under the impact of open canal flow rate, 2 calculation models were proposed. In the 1st model, we assumed that lift force was the vertical component of total static water pressure (pressure body) and based on the momentum theorem and the moment-equilibrium, the theoretical relationship between the deflection angle of the plate and the flow rate was deduced and tested in a U-shaped canal and a rectangular canal to verify the rationality of the theoretical formula. In the 2nd model, the flow pattern was analyzed and the formula for calculating the outlet flow of gate was applied to the flow relative to measuring device and the flow calculation model was established. The undetermined coefficients in the flow coefficient calculation model were estimated. The measuring device was installed at 5.0 m far from the inlet of upstream of U-shaped canal while 4.5 m far from the inlet in rectangular canal. The base slope of U-shaped canal was 1/2 000 while the zero slope in the rectangular canal. The triangular weir was installed at the end of the downstream of canals to measure current flow. Experiments and were performed for total 25 working conditions on the plate measuring devices with flow rate up to 44 L/s to verify calculation models. The results showed that both pressure body assumptions were applicable to flow calculation in the U-shaped canal. The relative error between calculated and measured flow was less than 10% except when the flow rate was less than 10 L/s. When the flow was greater than 17 L/s, the error was less than 5%. In the rectangular channel, only hypothesis 1 was applicable for flow calculation when the hypothesis 2 was invalid. Brake orifice discharge model developed for upstream depth versus discharge under different working conditions were satisfying with the relative error of 10% under most working conditions, which met the common requirements of flow measurement in irrigation areas. The flow measurement range was between 10 L/s and 44 L/s. When the size of draping thin plate was close to cross-sectional dimension of the canal, the flow rate and the deflection angle had a corresponding relationship. There were 2 water depth ratios, one of which was water depth ratio of upstream and downstream and the other was the ratio of water depth in front of the plate to downstream. Under the same flow rates, the 2 ratios decreased as an increase in the deflection angles. Under different flow rates, the 2 ratios increased as an increase in the deflection angles. The rationality of the model need further verification, when the canal size, water flow conditions, and plate shape changed. This study provided important information for flow measurement of terminal canals in irrigation areas.

Keywords: canal; angle; flow rate; flow resistance; stress direction; brake orifice outflow